

The chilled water production system of Gerland's bioproduction facility in Sanofi Lyon is being updated to :

- Meet the ongoing environmental challenges of reducing CO2 emissions
- Optimize its energy productivity ;
- Acquire more robustness and cold production capacity.

| Starting date of the project | October 2020: Study phase | | |
|--|---|--|--|
| Project Localisation | Sanofi Lyon Gerland, 23 bd Chambaud de la Bruyère 69007 LYON | | |
| Places of implementation of the project at this stage and targeted geography if replicable. | Replicability target: The target scope includes all French sites where a plan with a strong enough subsidy structure makes the project financially feasible. | | |
| Project objectives Type of climate innovation of the project with a description of the problem/issue addressed | Reduce the site's energy consumption and associated CO2 emissions by recovering the heat produced during the production of chilled water for re-use in the heating hot water networks. | | |
| Detailed project description | The principle of low-temperature heat recovery is one of the priorities of Sanofi's decarbonization approach. | | |
| | The project involves removing the old heat pump and replacing it with a new heat recovery c hiller that uses modern technology (magnetized bearings). | | |
| | The improvements have the following specific effects on how the site produces chilled water and heating hot water: | | |
| | > Original system operation | | |
| | Originally, the system consisted of the following equipment: - A heat pump (Heat pump) that operates continuously to produce chilled water and hot water. | | |
| | - The three current chillers (GF1, GF2 and GF3) take over to produce cold water in addition to the production of the heat pump. The chillers are switched on one after the other with an operating order that ensures an equivalent annual operating time between each chiller. | | |
| | - A steam-water exchanger located in LYG3, fed by the steam produced by the boiler in operation, which provides additional power for the production of hot water. This equipment currently supports the heat pump in order to produce the hot water necessary for heating the premises, mainly in winter. Thus, the overall production of cold water provided by this energy installation is intended to supply equipment such as air handling units (AHU), water loop exchangers, air conditioning cassettes, etc. | | |
| | - As for the production of hot water, it is mainly produced by the heat pump with, if necessary, the LYG3 exchanger as a support in order to heat the premises of the whole establishment (via AHU and air conditioning cassettes). | | |
| | > Operation of the new water production system | | |
| | - The project incorporates a new heat pump (620 kWp and 820 kW hot TFP) that will replace the existing equipment and operate to produce both chilled and hot water. This new equipment will be more energy efficient. | | |
| | - A new GF4 chiller (1414 kWp and 950 kW hot) which will be more efficient than the current equipment and will contribute to the production of cold water for the Sanofi Genzyme facility | | |

| | and will be equipped with a heat recovery system. Thus, via heat recovery, the GF4 will contribute to the production of hot water for the site. This new operation will make it possible to stop using the current steam exchanger during the winter period and thus reduce the consumption of gas from the boilers (carbon neutrality objective to ensure the global heating of the establishment). - The three current chillers (GF1, GF2 and GF3) will take over to produce additional cold water. | | | | | |
|--|--|---|--|--|--|--|
| | - The two new units, TFP and GF4, will be equipped with an HFO type R1234ze refrigerant (the previous TFP was initially equipped with an R134A fluid). | | | | | |
| | (the provides if if was initiality equipped with all those initiality). New chiller With heat recovery (n*4) GF 3 GF 2 Conservation of the 3 existing chillers Heat Pump Replacement of existing heat pump Keeting network | | | | | |
| | | | | | | |
| | The project (1.221 M€) was financed by the Energy Savings Certificates (CEE) up to 1.04 M€ and was carried by Engie (Equans) for CEE. | | | | | |
| | This waste heat recove | ry facility is fully operat | ional since December 2021. | | | |
| Main project's drivers for reducing the greenhouse | Reduction le | vers | Details on the aspects of the project | | | |
| gas emissions Enter the information in the appropriate boxes | □ Energy and (including bel | d resource efficiency naviour) | | | | |
| | ⊠ Energy Decarbonisation | | Use of waste heat from the new chiller for heating, replacing part of the other modes of hot water production: boilers and steam | | | |
| | | | exchanger. | | | |
| | ⊠ Energy ef improvemen | | exchanger. Greater energy efficiency of the two new equipments: the new TFP in comparison to the old, and the GF4 in comparison to the GF1, GF2, and GF3. | | | |
| | improvemen | ts efficiency in non- | Greater energy efficiency of the two new equipments: the new TFP in comparison to the old, and the GF4 in comparison to the GF1, | | | |
| | Improvemen □ Improving energy resou □ Emissions of carbon sint | ts efficiency in non- rces absorption: creation | Greater energy efficiency of the two new equipments: the new TFP in comparison to the old, and the GF4 in comparison to the GF1, | | | |
| | improvemen □ Improving energy resou □ Emissions of carbon sinl emissions (B □ Financing | ts efficiency in non- rces absorption: creation ks, negative | Greater energy efficiency of the two new equipments: the new TFP in comparison to the old, and the GF4 in comparison to the GF1, | | | |
| | improvemen □ Improving energy resou □ Emissions of carbon sinl emissions (Bl □ Financing or disinvestm assets ⊠ Reductior | ts efficiency in non- rces absorption: creation ks, negative <u>ECCS, CCU/S,)</u> ow-carbon producers ent from carbon | Greater energy efficiency of the two new equipments: the new TFP in comparison to the old, and the GF4 in comparison to the GF1, | | | |
| Emission scope(s) on which the project has a significant impact and quantification of GHG emission reductions per emission scope | improvemen □ Improving energy resou □ Emissions of carbon sinl emissions (BI □ Financing I or disinvestm assets ⊠ Reductior greenhouse | ts efficiency in non- rces absorption: creation ks, negative ECCS, CCU/S,) ow-carbon producers ent from carbon of other | Greater energy efficiency of the two new equipments: the new TFP in comparison to the old, and the GF4 in comparison to the GF1, GF2, and GF3. substitution of the R134A refrigeration fluid by R1234ZE (with a GWP roughly 200 times lower) in a new thermopompe, dramatically reducing emissions caused by leaks. t Quantification of associated GHG emissions | | | |

| | 1 F | 1 | 1 | | |
|--|---|---|--|--|--|
| considered (left-hand column) | Scope 1 | Substitution of R134a | Estimated at 40 tCO2 / year | | |
| and the quantification of associated emissions. | Direct | refrigerant by HFO R1234 ze with 200 times lower GWP. | (REX accidental leakage 2019 on heat pump) | | |
| associated emissions. | emissions generated by | with 200 times lower GWP. | 2019 on heat pump) | | |
| Indicate the main hypotheses | the | | | | |
| and calculation steps in the | company's | | | | |
| intended section (below the | activity. | | | | |
| table) | Scope 2 | | 109 teCO2 | | |
| | Indirect | Recovery of heat from the | | | |
| For further details, please | emissions | new cold group GF4 to heat | | | |
| refer to the methodology | associated | the building instead of using | | | |
| guidelines. | with the | the steam exchanger and gas | | | |
| | company's | boilers. | | | |
| | electricity | Greater electrical efficiency | | | |
| | and heat | from the new TFP and GF4. | | | |
| | consumption. | | | | |
| | Scope 3 | | | | |
| | Emissions induced | | | | |
| | (upstream or | | | | |
| | downstream) | | | | |
| | by the | | | | |
| | company's | | | | |
| | activities, | | | | |
| | products | | | | |
| | and/or | | | | |
| | services in | | | | |
| | its value | | | | |
| | chain. | l <u></u> | | | |
| | Increase of ca | arbon sinks | | | |
| | Emissions | | | | |
| | Absorption Carbon sinks | | | | |
| | creation, | | | | |
| | (BECCS, | | | | |
| | (<i>DE000</i> , <i>CCU/S</i> ,) | | | | |
| | GHG emissions avoided by the company at third parties | | | | |
| | Avoided | | | | |
| | Emissions | | | | |
| | Emissions | | | | |
| | avoided by | | | | |
| | the activities, | | | | |
| | products | | | | |
| | and/or | | | | |
| | services in | | | | |
| | charge of the | | | | |
| | project, or by the financing | | | | |
| | of emission | | | | |
| | reduction | | | | |
| | projects. | | | | |
| | | 1 | <u>.</u> | | |
| | Clarification on the | calculation or other remarks: | Based on the facility's 2019 | | |
| | consumption data a | and the outlook for increased ac | ctivity, it was estimated that the | | |
| | | t in the following consumption | | | |
| | | | estimates resulted in a projected | | |
| | | of 109 tCO2/year (conversion f | actor for nuclear energy and natural | | |
| | gas). | | | | |
| | | | | | |
| Modality of verification of the quantification. | Calculation standar | d used (ADEME base, GHG pro | (tocol, etc.): | | |
| the quantification. | Verification of the c | alculation (internal or external) | : internal factors based on nuclear | | |
| | | ral gas conversion factors. | | | |
| Other environmental and | | | sible to reduce the use of the site's gas | | |
| social benefits of the | | the possibility of using the vapor | | | |
| project | | | 5 | | |
| | | | | | |
| If possible, list the impacts | | | | | |
| and <u>Sustainable Development</u> | | | | | |
| Objectives concerned | | | | | |
| Project maturity level | Prototype laborato | | | | |
| | □ Real life testing (T | , | | | |
| Tick the corresponding | Pre-commercial pr | ototype (TRL 9) | | | |
| current maturity level | □ Small-scale impler | nentation | | | |
| | | | | | |

| | Medium to large scale implementation | | | |
|--|--|--|--|--|
| | | | | |
| | Demontres effets have to enter the level of maturity of the surgical | | | |
| Capacity and conditions of | Remarks: click here to enter the level of maturity of the project | | | |
| the project reproducibility, | ^^^ | | | |
| with associated climate | | | | |
| impact mitigation potential | | | | |
| Amount of investment made | Project amount of 1,221 M€: | | | |
| (in €) | - Financing from the CEE at a level of 1,045 M€ | | | |
| | - Financing provided by Sanofi up to €176,000. | | | |
| Economic profitability of | ⊠ ST (0-3 years) | | | |
| the project (ROI) | □ MT (4-10 years) | | | |
| | □ LT (> 10 years) | | | |
| | | | | |
| Engaged pertperahing | Remarks: click here to enter the information RAS – project purchasing | | | |
| Engaged partnerships Open comments from the | xxx | | | |
| project owner | | | | |
| | | | | |
| More about the project | | | | |
| Contact the company carrying the project | Aymeric.VIGNON@sanofi.com | | | |
| Please specify an ad hoc e- | | | | |
| mail address that will allow | | | | |
| the reader to contact the | | | | |
| project company directly | | | | |
| Project URL links | XXX | | | |
| Illustrations of the project | | | | |
| 3 photos/videos minimum (in HD format to be attached) | | | | |
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